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VERY LARGE AUTOTHERMAL REFORMERBACKGROUND OF THE INVENTION

5 An existing design for an autothermal reforming apparatus consists of a refractory lined, cylindrical vessel with a conical top part where the burner is installed in the top of the cone. The vessel is in principle divided into two zones, the top part being used as a flame chamber where combustion takes place and where also a high velocity swirling back-mix ensures an even  
10 temperature and composition at the inlet to the next zone where the filling of reforming catalyst takes care of equilibration of the reforming gas mixture.

This design is limited in capacity, mainly by two factors:

15 a. The refractory lined reactor can only be built up to a certain maximum diameter (maximum regarded to be for the moment approximately 7 m).

b. If the catalyst bed does not have enough flow area, the pressure drop over the catalyst bed will lead  
20 to risk of gas passing through the refractory lining or even behind the lining so that the pressure shell is overheated and damaged. (There are numerous examples from the industry that such a risk is real.)

SUMMARY OF THE INVENTION

25 The object of this invention is to provide a catalytic autothermal reactor which involves the following elements:

1. A combustion chamber which is empty and located inside the refractory lining of a vessel of similar shape as the one described above. The process burner through which the feed fluids are entering is mounted in the bottom of this combustion chamber and the mixed combustion products are leaving the top of the combustion chamber from where they are distributed to the following reactor(s).

2. One or more catalytic reforming reactors which are supplied with combustion product from the combustion chamber. The design of the catalytic reactor resembles the original design and by having more than one reactor, the capacity can be increased by a factor of 2 or 3 or more by having a sufficient number of such reactors connected to the combustion chamber where each reactor still respects the maximum allowable diameter.

#### BRIEF DESCRIPTION OF THE DRAWING

Appended hereto is a drawing, the sole figure of which schematically illustrates the preferred embodiments of the apparatus and process of this invention.

#### DESCRIPTION OF PREFERRED EMBODIMENTS

Referring to the drawing figure, there is provided a combustion chamber (1) having a burner (2) in the bottom thereof, provided with inlets (3) and (4) for introducing a hydrocarbon and steam feed mixture and oxidant, respectively. The combustion chamber (1) is open at the top (5) to a duct (6) which is provided with openings (7) and (8) for introducing the combustion products into

catalytic reforming reactors (9) and (10) having catalyst beds (11) and (12). The catalytic reactors (9) and (10) are provided with outlets (13) and (14) respectively at the bottoms thereof for the reformed product (syngas).

5 The reformed product is withdrawn via ducts (15) and (16), respectively, which communicate with a withdrawal duct (17).

The following example is illustrative of the process employing the apparatus of this invention.

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Example

Process gas flow entering into the burner, Nm<sup>3</sup>/h 800,000

Steam flow mixed into the feed flow, Nm<sup>3</sup>/h 480,000

Temperature of the mixed feed stream, °C 600

Pressure, bar 35

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Oxygen flow to burner, Nm<sup>3</sup>/h 480,000 at 300 °C and 35 bar

Temperature in the combustion chamber (reactor 1), °C 1320

Temperature at the exit of catalytic reactor  
reactor 2), °C 1050

Number of catalytic reactors: 4

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each with an internal diameter of 6-7 m

Besides obtaining the option to choose the plant capacity independent of the reactor diameter limitation, the present invention also makes it possible to supply the catalyst bed with gas which is arriving at a much  
25 lower linear velocity than what is otherwise necessary to obtain a good mixing, this because the mixing is now already obtained in the combustion chamber before the gas is distributed to the catalytic reactors. This reduces dramatically the risk of disturbances of the

catalyst bed top layer.

Although the present invention has been described  
in relation to particular embodiments thereof, many  
other variations and modifications and other uses will  
5 become apparent to those skilled in the art. It is  
preferred, therefore, that the present invention be  
limited not by the specific disclosure herein, but only  
by the appended claims.